

Mansoura University
 Faculty of Engineering
 Dept. of Power Mech. Eng.
 Course Title: Multi-Phase Flow
 Course Code: MPE6222



POST GRAD. STUDIES
 September 2013
 Exam Type: Final
 Time: 3 Hours
 Full Mark: 100

Answer all the following questions.

1) (a) Describe with drawing the operation principles of the two-phase air compressor [5 Marks]

(b) Beginning from the continuity equations for the liquid and the gas, prove that

$$U_G = G[xv_G + K(1-x)v_L] \quad \text{and} \quad U_L = \frac{G}{K}[xv_G + K(1-x)v_L]$$

where U_G , G , x , v_G , K , v_L and U_L are the gas velocity, the mass velocity, the dryness fraction, the gas specific volume, the velocity ratio, the liquid specific volume and the liquid velocity, respectively. [5 Marks]

(c) Prove that

$$\rho_H = 1 / [(x)/\rho_G + (1-x)/\rho_L]$$

where ρ_H , ρ_G , ρ_L and x are the homogeneous density, the gas density, the liquid density and the dryness fraction. [5 Marks]

(d) Liquid and gas flow in a 2 in. pipe. The values of the gas flow rate, the velocity ratio and the gas cross-sectional ratio (α) are 0.071 m³/sec, 11.2 and 0.4, respectively. Evaluate:

- (i) The phase velocities and homogeneous velocity.
- (ii) The slip velocity.
- (iii) The superficial phase velocities.
- (iv) The dryness fraction (x).
- (v) The mixture density and the homogeneous density.
- (vi) The single phase friction pressure gradients Dp_{FLO} , Dp_{FL} , Dp_{FGO} and Dp_{FG} . Take the single phase friction factor as $\lambda=0.19/Re^{0.2}$.
- (vii) The multipliers ϕ_{FLO}^2 , ϕ_{FL}^2 , ϕ_{FGO}^2 , ϕ_{FG}^2 taking the two-phase pressure gradient due to friction as 900 mbar/m.
- (viii) The physical property coefficient (Γ) and the normalized two-phase multiplier.

The physical properties are:

$$v_G = 0.84 \text{ m}^3/\text{kg}$$

$$v_L = 1 \cdot 10^{-3} \text{ m}^3/\text{kg}$$

$$\mu_G = 1.789 \cdot 10^{-5} \text{ N}\cdot\text{sec}/\text{m}^2$$

$$\mu_L = 1.002 \cdot 10^{-3} \text{ N}\cdot\text{sec}/\text{m}^2$$

[20 Marks]

2) (a) Discuss briefly the generalized (separated, dispersed and mixed) flow patterns for different fluid types. [5 Marks]

(b) Describe with drawing the flow patterns that can be occurred in vertical gas-solid flows in a circular duct. [5 Marks]

(c)- Describe with drawing the flow patterns that can be occurred in horizontal gas-liquid-liquid three phase flows in a circular duct. [5 Marks]

(d) Saturated steam enters a 40 mm pipe with a mass velocity of 200 kg/m²s and a pressure of 60 bars. Evaluate the pressure drop due to the momentum forces where:

1. the vapor is entirely condensed in the pipe.
2. the exit dryness fraction is 0.5 and the exit void fraction is 0.2.

The physical properties are

$$v_G = 32.4 \times 10^{-3} \text{ m}^3/\text{kg} \text{ and } v_L = 1.3 \times 10^{-3} \text{ m}^3/\text{kg} \quad [15 \text{ Marks}]$$

3) (a) Discuss briefly how the momentum flux can be measured. Also, evaluate the value of the velocity ratio at which the momentum flux will have its minimum value. [5 Marks]

(b) Specify the limitations of the Homogenous Flow Model. [5 Marks]

(c) Using the homogeneous theory and assuming that $\mu_{TP} = \mu_L$, prove that:

$$\Phi_{FLO} = \left[1 + \left(\frac{v_G}{v_L} - 1 \right) x \right]$$

where μ_{TP} , μ_L , Φ_{FLO} , v_G , v_L and x are the two-phase viscosity, the liquid viscosity, the two-phase multiplier, the gas specific volume and the liquid specific volume and the dryness fraction, respectively. [5 Marks]

(d) Two phase mixture of saturated steam and water is flowing in a vertical adiabatic pipe with 50 mm internal diameter and 3.5 m in length. Calculate the friction, gravity and momentum pressure drop in the pipe if the inlet mass velocity of steam and water are 500 and 700 kg/m².s, respectively. Assume constant properties at reference pressure $p = 7$ Mpa. The values of the void fraction, λ_{L0} and λ_{G0} are 0.2, 0.025 and 0.015, respectively.

$$\text{Where } \epsilon/D = 0.002 \text{ and } B_s = \begin{cases} \frac{21\Gamma - 2^{2-n} + 2}{\Gamma^2 - 1} & \text{when } \Gamma > 8.9 \\ 2^{2-n} - 1 & \text{when } \Gamma < 8.9 \end{cases}$$

$$\Phi_{FLO}^2 = 1 + (\Gamma^2 - 1) \left[B_x^{(2-n)/2} (1-x)^{(2-n)/2} + x^{2-n} \right]$$

$$\frac{B_R}{B_S} = \left[0.5 \left\{ 1 + \left(\frac{\mu_G}{\mu_L} \right)^2 + 10^{-600\epsilon/D} \right\} \right]^{(0.25-n)/0.25}$$

where B_R and B_S and n are the B coefficient parameter for rough and smooth pipes, respectively. n is the Blasius equation exponent.

The physical properties at reference pressure = 7 Mpa are

$$v_G = 32 \cdot 10^{-3} \text{ m}^3/\text{kg}, v_L = 1.0 \cdot 10^{-3} \text{ m}^3/\text{kg}, \mu_L = 100 \cdot 10^{-6} \text{ N.s/m}^2 \text{ and } \mu_G = 20 \cdot 10^{-6} \text{ N.s/m}^2$$

Also, compare the total pressure drop with single-phase flow case, if:

- Only saturated water with $G = 1200 \text{ kg/m}^2 \cdot \text{s}$ was flowing in the same pipe,
- Only saturated steam with $G = 1200 \text{ kg/m}^2 \cdot \text{s}$ was flowing in the same pipe. [20 Marks]

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