

CALCULATIONS OF TEMPERATURE DECAY FOR INDUSTRIAL CHIMNEY BY USING MODIFIED ANALYTICAL MODEL

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Abstract

The engineering design of industrial chimneys requires predicting the temperature decay of exhaust gases along the walls of chimney. This paper investigates the practical calculation of the thermal performance of industrial chimneys which leads to estimating the static draft and the bulk temperature of combustion gases at the chimney's exit for determining the air pollution levels in the vicinity of the stack.

A modified analytical model is used to obtain accurate heat transfer results. Heat transfer processes involving the internal convection heat transfer, external heat transfer to the surrounding and conduction heat transfer, which takes into account fouling resistance are considered.

The present modified analytical model provides a good estimation of the bulk temperature and the outside wall temperature compared with that computed using 1-D lumped model (Cortes model). The present modified model is validated with published theoretical and experimental data. The validation shows that the present modified model is more accurate than 1-D lumped model (Cortes model). The paper describes the thermal calculation procedures of industrial chimneys using the standard heat transfer correlations. The calculation procedures are easy to apply by design engineers in the field of thermal design of chimneys. Also, comparison between the present modified model and the previous 1-D lumped model with recent experimental data measured at the glass furnace chimney at El-Araby for Lighting Technology (glass factory) is discussed.

إن التصميم الهندسي للمداخن الصناعية يتطلب التنبؤ بالإندثار الحراري لغازات العادم علي طول جدران المداخن. إن هذا البحث يفحص الحسابات العملية للأداء الحراري للمداخن الصناعية والتي بدورها تؤدي إلي تحديد السحب الإستاتيكي، ودرجة حرارة غازات العادم عند مخرج المدخنة لتحديد نسبة تلوث الهواء بمحيط المدخنة.

لقد تم إستخدام نموذج تحليلي معدل من أجل الحصول علي نتائج دقيقة لإنتقال الحرارة. إن عمليات إنتقال الحرارة بالمداخن تتضمن إنتقال الحرارة الداخلي، وإنتقال الحرارة للمحيط الخارجي، وإنتقال الحرارة بالتوصيل والتي تأخذ في الإعتبار مقاومة الترسيب.

ولقد أعطى النموذج التحليلي المعدل تحديد جيد لدرجات الحرارة في الداخل والتوزيع الحراري علي الجدار الخارجي مقارنة بالنموذج الإجمالي ذات البعد الواحد (نموذج كورتس). ولقد تم التأكد من صلاحية النموذج المعدل من خلال مقارنته بنموذج كورتس وأيضاً مقارنته بقياسات فعلية؛ هذا الإختبار وضح أن النموذج المعدل يعطي نتائج أدق من نموذج كورتس. يصف البحث الإجراءات المتبعة في الحسابات الحرارية للمداخن الصناعية. حيث إستخدمت العلاقات القياسية لإنتقال الحرارة في حسابات هذا النموذج. وتعد الإجراءات الحسابية للتصميم الحراري للمداخن لهذا النموذج أسهل في الإستخدام بواسطة مهندسي التصميم. أيضاً تم مطابقة ومناقشة هذا النموذج الجديد المعدل بقياسات عملية لمصنع العربي للزجاج وأعطت نتائج جيدة.

KEYWORDS: Draught system, Chimney design, Modified model, El-Araby chimney, Chimney calculation

Nomenclature

| | | | |
|------------|---|---------------|--|
| A_i | inner cross-sectional area of the duct | h_i | local, internal convective coefficient |
| C_{pi} | specific heat of combustion gases | k_e | thermal conductivity of air |
| D_e | outside diameter of chimney | k_i | thermal conductivity of flue gas |
| D_i | inside diameter of chimney | k_w | thermal conductivity of the chimney wall |
| g | acceleration of gravity | k_f | fouling thermal conductivity |
| $Gr_{e,L}$ | external Grashof number based on $L, g \beta_e (T_{w,e} - T_\infty) L^3 / \nu_e^2$ | k_{st} | thermal conductivity of steel |
| h_e | local, external convective coefficient | k_{ins} | thermal conductivity of insulation |
| | | f | friction factor |
| | | L | axial station; chimney height |
| | | $\frac{L}{D}$ | dimensionless L, $L/R_i Pe_i$ |

| | |
|-----------------------|---|
| m | flue gas mass flow rate |
| Nu_e | local, external Nusselt number, $h_e D_e / k_e$ |
| $\overline{Nu_e}$ | streamwise mean of Nu_e |
| $\overline{Nu_{e,L}}$ | streamwise mean Nusselt number based on height L , $(L/D_e)Nu_e$ |
| Nu_{eq} | local, equivalent Nusselt number, UD/k_i |
| $\overline{Nu_{eq}}$ | streamwise mean of Nu_{eq} |
| Nu_i | local, internal Nusselt number, $h_i D_i / k_i$ |
| $\overline{Nu_i}$ | stream wise mean of Nu_i |
| Pe_i | Péclet number, $Re_i Pr_i = 4m C_{pi} / k_i \pi D_i = w D_i / \alpha_i$ |
| Pr_e | Prandtl number of the ambient air |
| Pr_i | Prandtl number of the flue gas |
| q_r | radiative heat flux |
| r | radial coordinate |
| R | chimney radius |
| R_i | inner radius |
| $Ra_{e,L}$ | external Rayleigh number based on L , $g \beta_e (T_{w,e} - T_\infty) L^3 / \nu_e \alpha_e$ |
| $Ra_{e,o}$ | external Rayleigh number based on inlet temperature, $g \beta_e (T_o - T_\infty) D_e^3 / \nu_e \alpha_e$ |
| $Ra_{e,w}$ | external Rayleigh number based on wall temperature, $g \beta_e (T_{w,e} - T_\infty) D_e^3 / \nu_e \alpha_e$ |
| Re_e | external Reynolds number based on wind velocity, $u_\infty D_e / \nu_e$ |
| Re_i | internal Reynolds number, $4m / \mu_i \pi D_i = u D_i / \nu_i$ |
| $T(r,z)$ | local temperature of combustion gases |
| T_b | bulk temperature of combustion gases |
| T_o | flue gas inlet temperature |
| T_r | effective radiating temperature of the surroundings |
| T_w | wall temperature |
| $T_{w,e}$ | outer surface temperature |
| $T_{w,i}$ | inner surface temperature |
| T_∞ | ambient air temperature |
| U | local, overall heat transfer coefficient |
| u_∞ | wind velocity component normal to the chimney axis |
| $V(r)$ | axial velocity of combustion gases |
| z | axial coordinate |

| | |
|-------|----------------------------------|
| Z | dimensionless z , $z/R_i Pe_i$ |
| G_z | Graetz number |

Greek symbols

| | |
|----------------|---|
| α_e | air thermal diffusivity |
| α_i | thermal diffusivity of combustion gases |
| β_e | thermal expansion coefficient of air |
| ϵ_e | outside wall emissivity |
| k_e | thermal entrance factor |
| k_p | temperature profile factor |
| k_t | transition regime factor |
| γ_i | dynamic viscosity of the combustion gases |
| ν_i | kinematic viscosity of the combustion gases |
| ν_e | air kinematic viscosity |
| θ_b | dimensionless T_b , $(T_b - T_\infty) / (T_o - T_\infty)$ |
| θ_w | dimensionless T_w , $(T_w - T_\infty) / (T_o - T_\infty)$ |
| $\theta_{w,e}$ | dimensionless $T_{w,e}$, $(T_{w,e} - T_\infty) / (T_o - T_\infty)$ |
| $\theta_{w,i}$ | dimensionless $T_{w,i}$, $(T_{w,i} - T_\infty) / (T_o - T_\infty)$ |
| ρ_i | combustion gases density |
| σ | Stephan-Boltzmann constant |
| ξ | transverse curvature coordinate |

Subscripts

| | |
|---------|------------------------------|
| e | ambient air; outer side |
| i | combustion gases; inner side |
| L | based on length L |
| w | wall |
| cyl | cylinder |
| $forc$ | forced convection |
| $plate$ | flat plate |
| mix | mixed convection |
| $free$ | natural convection |
| rad | thermal radiation |
| g | combustion gases |

1. INTRODUCTION

The chimney is an important structure in the industrial activities which use conventional fuels. Chimney is the last structure in the flue gases path and used for removing pollutants resulting from the combustion of fuel. It safeguards people at or close to the zone from high concentrations of those pollutants by providing dilution of the pollutants in the atmosphere. Chimney structures should be able to contain this flue gas without being deteriorated. At present time many considerations are taken into account to estimate the static draft and the bulk temperature at the chimney exit. Therefore, the effective acid dew point can be driven as high as (115°C- 140°C), Cortes and Campo [1].

Furthermore, the risk of acid deposition on the inner wall should be avoided for some fuels by preventing flue gases from condensing. If the flue gases temperature goes down and reaches to the dew point that causes acids condensation and wall corrosion. These are realistic problems in industries and power plants that utilized in boilers and combustion chambers for their processes, where high temperature of flue gases is discharged through a chimney and the flue gases exit temperature is therefore very important. For that, Heat

transfer through chimney wall should be considered in chimney design. The exchange of heat between the outer surface of chimney and the surrounding air depends on wind velocity. Also, thermal radiation contributes in external heat transfer process especially for cases characterized by free convection. Few studies about chimneys design and their calculations were investigated. The one dimensional lumped model was used to calculate the heat transfer and the temperature gradient along the chimney.

Cortes and Campo [1] describes the design criteria for thermal calculation of industrial chimneys. They applied a 1-D lumped formulation which takes into account the axial variations of the inner and outer Nusselt numbers. The calculation of the axially mean bulk temperature has been performed iteratively by evaluating a single exponential function.

Parallel theoretical and numerical analysis has been conducted for the prediction of the mean bulk temperature. A two-dimensional lumped model with comparison between theoretical and numerical results was done by Campo [2].

Maref et al. [3] presented numerical simulation of thermo-convective behavior of smoke conduit. The good agreement between computed and measured temperatures leads to the conclusion that numerical model is able to predict qualitatively the thermal distribution in the conduit.

The relations between many parameters of chimney were studied by Ming Chu et al. [4]. Cold inflow was demonstrated using data obtained for an electrically heated model natural draft air-cooled heat exchanger to impair the solid chimney height by up to 90 percent without wire mesh protection and 60 percent with wire mesh protection.

A semi-empirical correlation for pressure drop is developed from a theoretical base by first making use of the momentum integral solution to the heat and momentum equations for natural convection on a vertical surface by Joye [5]. Some assumptions were taken into consideration during the study such as the boundary condition on the free-stream side of the boundary layer which is changed to reflect the shear on that surface due to the forced convection. The empirical data were used to develop a formula that is useful in design and applications.

Natural convection from a vertical electrically heated plate, placed in a chimney, has been investigated experimentally and numerically by Kazansky et al. [6]. Effect of chimney height on heat transfer rates from the plate and also on the temperature and flow

fields inside the chimney has been studied in details. Local mean fluctuating temperatures and velocities have been experimentally obtained for various locations inside the chimney. Along the flow visualization, a comprehensive picture of the phenomena is obtained. This study showed that the temperature of air at any point above the plate decreases considerably as the height of the chimney increases.

Campo et al. [7] were conducted a semi analytical analysis for the prediction of the mean bulk and interface temperatures of gaseous and liquid fluids moving at high pressures inside thick walled metallic tubes with isothermal conditions at the outer surface. The one-dimensional and two-dimensional lumped models were examined for the thermal response of this kind of tube in-flow. The computed results showed that 1-D lumped model is more accurate than 2-D lumped model.

Belver et al. [8] were investigated a simplified fluid structure interaction approach by using computational fluids dynamics. This approach was used to study the dynamic behavior of a particular 90 m steel chimney under vortex-induced vibrations. The results presented new possibilities in the field of structural assessment and control simulation.

The design rules for cross-wind vibrations are given by design models codes. Verboom et al. [9] studied three design rules and carried out tests on 13 industrial chimneys. The results showed that approach 3 gives a good indication of the stresses due to cross- wind vibrations.

Kawecki and Zuranski [10] studied a Cross-wind vibrations of a new steel chimney 100m high caused twice damage of bolts. The damping properties were measured of the chimney and were permitted to compare different approaches to the calculation of relative amplitude of vibration. This practical example was given evidence that better description of crosswind vibrations is the calculation procedure given as Approach 2 in Euro code.

Numerical investigation of transient natural convection in a vertical channel-chimney system symmetrically heated at uniform heat flux has been investigated by Andreozzi et al. [11]. This study was carried out by using finite volume method. It was showed a comparison among the maximum wall temperatures for all configurations with chimney and the simple channel pointed out which was the most critical configuration at steady state condition. The

results showed that the best configuration during the transient heating due to the lowest first overshoots. Bahadori and Vuthaluru [12] had been developed an Estimation of energy conservation benefits in excess air controlled gas-fired systems. This method was used to predict the natural gas efficiency in boilers and other gas-fired systems related to excess air and exhaust gases.

In many industries such as glass melting industry, the deposits material is an important factor. These materials have been carried by the exhaust gases out from the furnace. Ruud et al. [13] have been analyzed the types of fouling materials out from the glass furnace and determine the thermal conductivity of it. The aim of this study focuses on calculation of the bulk temperature at the chimney exit and temperature distribution along the chimney axial length for the inner and outer side of chimney based on a modified analytical model. The present modified model is validated with published 1-D lumped model and experimental data. Also, this paper makes a comparison between the present modified model and 1-D lumped model with experimental data measured for an actual case at El-Araby glass melting furnace.

2. Mathematical model

Heat transfer processes for the combustion gases inside chimney is involving internal forced convection and external heat transfer to the surroundings. There are different methods to simulate this problem and know the temperature decay and distribution along the chimney's length. One-Dimensional lumped model is presented by Cortes and Campo [1] to estimate the mean bulk temperature at the exit of chimney. A two dimensional lumped model, partial differential energy equation subjected to a nonlinear convective boundary condition via a simple solution for a uniform temperature is used to compare the results from 1-D lumped model by Campo [2]. The present modified lumped model is suggested to improve the results of the temperature distribution along the industrial chimneys and this model is validated with the Cortes model results [1].

2.1 Cortes model

Regarding to Cortes and Campo model [1] which considered both the external and internal heat transfer and has been done by using dimensionless groups, the internal Nusselt number correlation for turbulent forced convection is a function of Reynolds number (Re_i) and Prandtl number (Pr_i) and it is given by:

$$\overline{Nu}_i = k_t k_p k_e \frac{0.023 Pr_i^{0.9} Re_i^{0.8}}{\left(1 + \frac{Pr_i^{1.7}}{Re_i^{0.3}}\right)^{1/3}} \quad (1)$$

Where k_t , k_p and k_e are transition regime factor, temperature profile factor and thermal profile factor respectively.

Free convection from outer chimney walls has been calculated by Churchill and Chu [14] as follow:

$$\overline{Nu}_{e,L} = \left[0.825 + \frac{0.387 Ra_{e,L}^{1/4}}{\phi(Pr_e)}\right]^2 \quad (2)$$

$$\text{Where, } \phi(Pr_e) = \left[1 + (0.492/Pr_e)^{9/16}\right]^{8/27} \quad (3)$$

For an isothermal wall $Ra_{e,L}$ is the Rayleigh number based on the height L:

$$Ra_{e,L} = \frac{g \beta_e (T_{we} - T_{w\infty}) L^3}{\nu_e \alpha_e} \quad (4)$$

The external Nusselt number for forced turbulent flow convection by using the classical correlations of Zukauskas and Coworkers [15]

$$\overline{Nu}_e = 0.023 Re_e^{0.8} Pr_e^{0.4} \quad (5)$$

Equation (5) can be used for an isothermal cylinder in cross flow in the range ($2 \times 10^5 < Re_e < 2 \times 10^6$)

Where $Re_e = u_\infty D_e / \nu_e$ is the Reynolds number based on the outside diameter and (u_∞) is the wind velocity. The wind velocity is assumed to be perpendicular to the chimney axis. The equivalent Nusselt number as a function of internal Nusselt number, external Nusselt number and the thermal conductivity of the wall can be presented as follows:

$$\frac{1}{\overline{Nu}_{eq}(L)} = \frac{1}{\overline{Nu}_i(L)} + \frac{1}{k_e} \frac{1}{k_i \overline{Nu}_e(L)} + \frac{1}{2} \frac{k_i}{k_w} \ln \frac{D_e}{D_i} \quad (6)$$

Where, $Nu_{eq} = UD_e / k_i$

2.2 Present Modified Analytical model

In this model, the chimney is considered as a heat exchanger. The modified analytical model uses the bulk temperature relation which is a function of the overall heat transfer coefficient, mass flow rate of flue gases, heat capacity of flue gases and area. The modified model is applied more adequate correlation to be near to the fact. The overall heat transfer coefficient involves internal and external heat transfer coefficients. Not only the convection and the radiation heat transfer are considered in the calculation of overall heat transfer coefficient but also heat transfer by conduction is added. Heat transfer by conduction includes fouling resistance, insulation resistance and wall resistance. Also, the present modified model uses a new correlation for internal Nusselt number. This correlation includes the friction factor in addition to Reynolds and Prandtl numbers. The change of gas temperature can be expressed by the following first order differential equation [1]:

$$\frac{dT_{bz}}{dz} = -\frac{UzD}{m \cdot Cp_i} (T_b - T_\infty) \quad (7)$$

Where (m') is the mass flow rate, (V) is the velocity of gases, (T_∞) is the surrounding air temperature and (T_g) is the gas temperature. The heat transfer resistances can be expressed as an in-series thermal circuit, involving the inside and outside convection coefficients (h_i , h_e) and thermal conductivity resistance of wall including the fouling resistance.

The overall heat transfer coefficient (U) is defined as follow:

$$\frac{1}{UA_e} = \frac{1}{h_i A_i} + \frac{1}{h_e A_e} + R_{t,wall} \quad (8)$$

Through integrating equation (7), the gas temperature distribution along the chimney may be given by:

$$T_{b(z)} = \frac{\int \rho_i V Cp_i T dA}{m \cdot Cp_i} = \frac{\int V T dA}{V dA} \quad (9)$$

Where (T_o) is the gas temperature at inlet to chimney (zero position).

The assumptions which are usually used for equations (7) and (9): low velocity, incompressible flow and neglect the change of density and heat capacity due to the temperature decay along the chimney duct. According to [1] the following dimensionless variables and parameters are used.

$$\bar{L} = \frac{L}{Re_i Pe_i} \quad (10-a)$$

$$\theta_b(\bar{L}) = \frac{T_b - T_\infty}{T_o - T_\infty} \quad (10-b)$$

$$Nu_{eq} = \frac{U D_i}{k_i} \quad (10-c)$$

where k_i is the thermal conductivity of flue gases and Pe_i is the Péclet number ($Pe_i = Re_i Pr_i$). Therefore equation (7) becomes:

$$\frac{d\theta_b}{d\bar{L}} = -2 [Nu_{eq}(\bar{L})] \theta_b \quad (11)$$

By integrating equation (11), the bulk temperature distribution is as follows:

$$\theta_b(\bar{L}) = \exp \left\{ -2 \left[\overline{Nu_{eq}}(\bar{L}) \right] \bar{L} \right\} \quad (12)$$

Likewise, it is easy to present the relation of the dimensionless wall temperature as follows:

$$\theta_w(\bar{L}) = \theta_b \left(1 - \frac{Nu_{eq}}{Nu_i} \right) \quad (13)$$

Then, inner wall and outer wall temperatures can be expressed as follows:

$$\theta_{w,i}(\bar{L}) = \theta_b \left(1 - \frac{Nu_{eq}}{Nu_i} \right) \quad (14)$$

$$\theta_{w,e}(\bar{L}) = \frac{\theta_b}{k_e/k_i} \left(\frac{Nu_{eq}}{Nu_e} \right) \quad (15)$$

The external Nusselt number correlation available in the literature has been used in the present modified model as given in [1]. Although buoyancy forces do exist due to the change of gas density with temperature along the stack, in this model inner buoyancy effects will be negligible compared with

radiation effects. Under calm conditions, the chimney is cooled by a flow of air driven by natural convection. Radiation heat transfer may be then of a comparable order of magnitude, depending on the effective radiating temperature of the surroundings and the wall emissivity. On the other hand, for outside walls forced convection caused by the high speed wind is tested. The inside and outside correlations of convection are presented [16]. The equivalent Nusselt number modifies to take into account a thick tube wall, as in the cases of a stack made of brick or a layer of thermal insulation. The equivalent Nusselt number is defined as follows [1]:

$$\frac{1}{Nu_{eq}(L)} = \frac{1}{Nu_i(L)} + \frac{1}{k_w/k_i} \frac{1}{Nu_e(L)} + \frac{1}{2} \frac{k_i}{k_w} \ln \frac{D_e}{D_i} \quad (16)$$

where the local equivalent Nusselt number ($Nu_{eq} = UD_e/k_i$), the internal and external Nusselt numbers referring to the duct diameter, ($Nu_i = h_i D_i/k_i$), ($Nu_e = h_e D_e/k_e$), and the ratio of thermal conductivities of external and internal (k_e/k_i).

Also, overall heat transfer coefficient (U) can be expressed in the following manner:

$$U = \frac{1}{A_{inside} \left[\frac{1}{(hA)_{inside}} + R_{t,wall} + \frac{1}{(hA)_{outside}} \right]^{-1}} \quad (17)$$

2.2.1 Internal heat transfer coefficient

The Graetz correlation [16] presents heat transfer coefficient in turbulent flow pipe which is used to calculate the internal heat transfer coefficient in modified model. This correlation takes in to account the roughness of pipe which is a function of friction factor (f) [17]. In case of laminar flow ($Re_i < 2300$), the inner Nusselt number can be presented as follows:

$$\overline{Nu}_i = 3.657 + \frac{0.0668 G_z^{1/3}}{0.04 + G_z^{-2/3}} \quad (18)$$

where Graetz number can expressed as follows:

$$G_z = \frac{Re_i Pr_i D_i}{X_i} \quad (19)$$

The first step to calculate the heat transfer coefficient inside the duct is to calculate Reynolds number based on inner diameter as follows:

$$Re_i = \frac{\rho_{av} D_i v_g}{\mu_g} \quad (20)$$

Equation (18) is used to calculate internal Nusselt number for laminar flow in chimney duct. As for turbulent flow ($2300 \leq Re_i < 5 \times 10^6$), the Nusselt number is a function of Prandtl number, Reynolds number and friction factor. Internal Nusselt number can be given by [16]:

$$\overline{Nu}_i = \frac{(f/g)(Re_i - 1000) Pr_i}{1 + 12.7 \sqrt{f/g} (Pr_i^{2/3} - 1)} \quad (21)$$

The internal heat transfer coefficient can be then expressed as follows:

$$\bar{h}_i = \frac{Nu_i k_i}{D_i} \quad (22)$$

2.2.2 Chimney wall thermal resistances

In present study the range of realistic conditions given about a certain case study, both internal and external flows will be considered. Under this premise, the effect of thermal conductivity of fouling layer is too important in addition to the thermal conductivities of insulation and wall layers. These conduction resistances should be taken into account as boundary conditions in this problem to be more real and to firm guarantee of the accuracy of the present analytical model. Assuming that the thermal conductivity of the wall is k_{st} , the thermal conductivity of insulation is k_{in} and the fouling thermal conductivity is k_f as shown in figure (1).

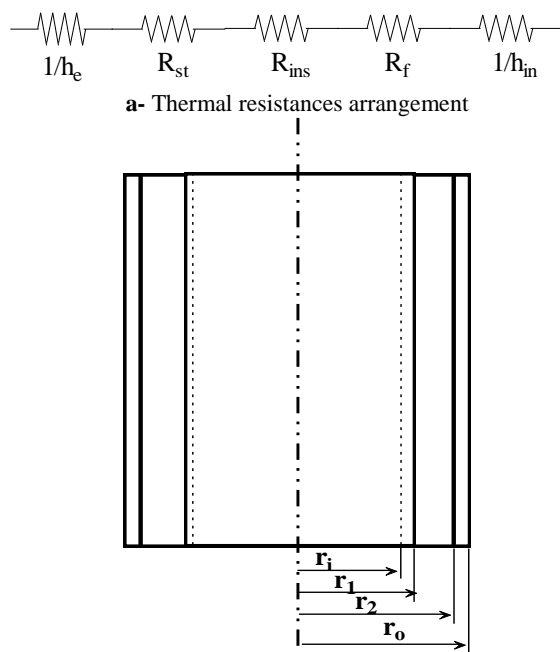


Fig.1.Chimney wall resistances

i. Steel wall conduction resistance:

In industrial chimneys, the outside wall layer is always made of steel and the thermal resistance is given as:

$$R_{st} = \frac{1}{2\pi k_{st} L} \ln \left(\frac{r_o}{r_2} \right) \quad (23)$$

where (r_2) is the steel wall inner radius, (r_o) is the outer radius of steel wall and (L) is chimney's length.

ii. Insulation conduction resistance:

In industrial furnaces, chimney's insulation is used. The materials are thermal brick, aluminum silicate and some materials which have low thermal conductivities. The importance of thermal insulation comes back on the economic studies which prevent heat loss to the ambient. Insulation thermal resistance is given by:

$$R_{ins} = \frac{1}{2\pi k_{in} L} \ln \left(\frac{r_2}{r_1} \right) \quad (24)$$

where (r_1) is the inner radius of thermal insulation.

iii. Fouling conduction resistance:

After a long period of its working, most of industrial chimneys exposed to some of fly ashes which are accumulated and deposited on chimney's inner walls. These ashes form a fouling layer. This fouling layer increases with the time. Also, it will increase the conduction resistances. The fouling resistance can be expressed as follows:

$$R_f = \frac{1}{2\pi k_f L} \ln \left(\frac{r_1}{r_i} \right) \quad (25)$$

Where (r_i) is the fouling inner radius
Then the total conduction resistance is,

$$R_{tot,cond} = R_{st} + R_{ins} + R_f \quad (26)$$

2.2.3 External heat transfer Coefficient

The chimney outside walls is exposed to the low ambient conditions. The present study will focus on natural convection effect and it will take into account wind speed effect. Whenever the boundary layer thickness is much thinner than the cylinder radius, curvature effects are negligible. The heat transfer on outside wall is divided to heat transfer due to free convection, heat transfer due to thermal radiation and heat transfer due to forced convection.

a- Due to free convection

The most popular correlation of free convection has been defined by Churchill and Chu [14] and can be expressed as follows:

$$\overline{Nu}_{e,L} = \left[0.825 + \frac{0.387 Ra_{e,L}^{1/4}}{\varnothing(Pr_e)} \right]^2 \quad (27)$$

$$\text{where } \varnothing(Pr_e) = \left[1 + (0.492/Pr_e)^{1/4} \right]^{8/27} \quad (28)$$

$$Ra_{e,L} = \frac{g \beta_e (T_w - T_w^\infty) L^3}{\nu_e \alpha_e} \quad (29)$$

and (ν_e , α_e , β_e , Pr_e) are known from air tables.

Equation (29) is valid for ($Ra_{e,L} \leq 10^{12}$).

If $Ra_{e,L} > 10^{12}$, it is originally formulated and calculated as [18] and always exists and appears in

tall chimneys. Also, this is a restrictive condition for the geometry of a vertical tube, so that correction factors have been proposed to calculate the effects of curvature of the tube [1]

$$\gamma(\xi) = \frac{(\overline{Nu}_e)_L \text{ cyl.}}{(\overline{Nu}_e)_L \text{ plate}} = \frac{1.034 - 0.025\xi + 0.136 \ln Pr_e}{1 - 0.197\xi + 0.017\xi^2 + 0.156 \ln Pr_e} \quad (30)$$

where ξ is transverse curvature coordinates and can be expressed as follows:

$$\xi = 4\sqrt{2} \left(\frac{L/D_e}{Ra_{e,w}} \right)^{1/4} \quad (31)$$

The Nusselt number for air which includes the effect of fluid properties and curvature is given by:

$$\overline{Nu}_e = 0.150 \frac{Ra_{e,o}^{1/3} \theta_{w,e}^{1/3}}{[\phi(Pr_e)]^2} \gamma(\xi) \quad (32)$$

$$\text{where } Ra_{e,o} = Ra_{e,w} / \theta_{w,e}$$

and $\theta_{w,e} = (T_{w,e} - T_\infty) / (T_o - T_\infty)$.

With regarding to the computational procedures used, these correlations may be recasted into a compact and general formula for the external Nusselt number as follows:

$$\overline{Nu}_e = \left(D_e / L \right) \overline{Nu}_{e,L} \quad (33)$$

In our calculations the Rayleigh number ($Ra_{e,o}$) is based on the entrance temperature (T_o) is preferred than the Rayleigh number ($Ra_{e,w}$) based on the wall temperature ($T_{w,e}$). This decision is advantageous because ($Ra_{e,o}$) is a fixed quantity and remains invariant during the cooling process.

b- Due to thermal radiation

The chimney exchanges heat through thermal radiation as a consequence of the interaction with ambient radiation sink. The total external Nusselt number is affected with thermal radiation of ambient under calm conditions. Just as considered mild temperature decay and a quasi isothermal wall, it is important to add radiation effects to free convection in external Nusselt number. This can be formulated as follows [19]:

$$\overline{Nu}_e = (\overline{Nu}_e)_{\text{free}} + (\overline{Nu}_e)_{\text{rad}} \quad (34)$$

The second term of radiation in equation (34) is given by:

$$q_r = \varepsilon_w \sigma (T_{w,e}^4 - T_r^4) \quad (35)$$

Where (ε_w) is the wall emissivity, (σ) is the Stephan-Boltzmann constant $5.67 \times 10^{-8} \text{ W/m}^2 \cdot \text{K}^4$

(T_r) is the effective radiating temperature of the surroundings which can be always considered to be equal to the surrounding temperature ($T_r \approx T_\infty$).

The radiation Nusselt number formula yields to be:

$$(\overline{Nu}_e)_{\text{rad}} = \frac{D_e q_r}{k_e (T_{w,e} - T_\infty)} = \frac{\varepsilon_w D_e \sigma (T_{w,e}^4 - T_r^4)}{k_e (T_{w,e} - T_\infty)} \quad (36)$$

The calculations which are considering natural convection only leads to different temperature decay profiles. On the other hand by adding thermal radiation to the external heat transfer coefficient this arrives to the nearest actual profile of the temperature distribution along the chimney outside walls.

c- Due to forced convection

In some applications, wind speed should be considered. Wind is an important role in design of tall chimney. It exerts static and dynamic loads (for tall chimney > 150m height). For that, wind is essentially in calculations of external heat transfer. Forced convection correlation made for an isothermal cylinder in cross flow is presented by Zukauskas and Ziugzda [15].

In the range of ($2 \times 10^5 < Re_e < 2 \times 10^6$),

$$\overline{Nu}_e = 0.023 Re_e^{0.8} Pr_e^{0.4} \quad (37)$$

Where Re_e is the Reynolds number based on the outside diameter (D_e) and the wind velocity (u_∞). It should be noted that the outside Nusselt number is constant in this case. For the usual range of parameters, the contribution of forced convection due to the wind is much larger than both natural convection and thermal radiation. For low wind velocities, however, the simultaneous contribution of the three mechanisms may be envisaged to know the states of convection heat transfer for the outside walls. A criterion for appraising the relative importance of convection effects for gases is given in Mills [20]. The cases of external convection can be expressed as follows:

$$Gr_{e,L} / Re_e^2 \begin{cases} \ll 1 & \text{forced convection} \\ \approx 1 & \text{mixed convection} \\ \gg 1 & \text{natural convection} \end{cases}$$

Now, there are two models that can be used to know the temperature decay along the chimney length. These models are used to aid the designers to know the exit temperature from chimney to prevent the flue gases condensation. The main differences between two models are as follows: in Cortes model internal Nusselt number is a function in the internal Reynolds number and the internal Prantle number. In the present modified lumped model the internal Nusselt number is a function of internal Reynolds number, internal Prantle number and the friction factor. The losses due to friction should be considered to

improve the temperature decay along the chimney length. Also, for the conduction resistance in the present modified model, the fouling layer is considered which will be formed after a period of time of operation. This will improve the prediction of temperature distribution to be more accurate than Cortes model.

3. Validation of the modified analytical model

Thermal power plants which are used coal as a fuel, the combustion products contain high amounts of SO₂ and other pollutants. Therefore, high stacks are needed. These chimneys are made of concrete or mineral material. The temperature distribution along chimney was measured on coal fired power plant (Teruel Power Station-Spain). Cortes model [1] is applied on this actual case and the results are compared with measured data under the following conditions: $T_{\infty}=18.98^{\circ}\text{C}$, $u_{\infty}=5\text{m/s}$, $T_0=191.678^{\circ}\text{C}$, $\dot{m}=1196.7\text{ kg/s}$, $D_i=19.1\text{ m}$, $L=343\text{ m}$, $k_w=1.5\text{ W/m.K}$.

Also, the present modified model is applied on this chimney at the same previous conditions to validate it. The comparison between the two models and measured data are shown in figure (2).

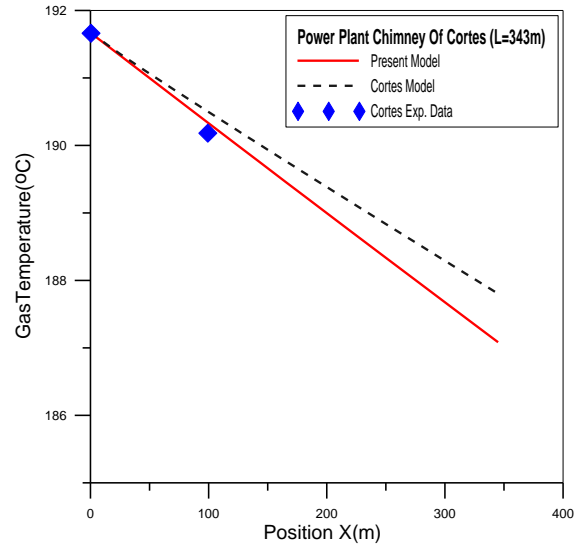


Fig.2. Validation curve

It can be observed that the present modified model gives good results agreed well with measured data more than Cortes model [1]. The reason of this good agreement of the present modified model with experimental results that the present model used internal Nusselt number based on (Re, Pr, f) and also, it considered the fouling resistance resulting from deposits formed by the exhaust gases that makes a

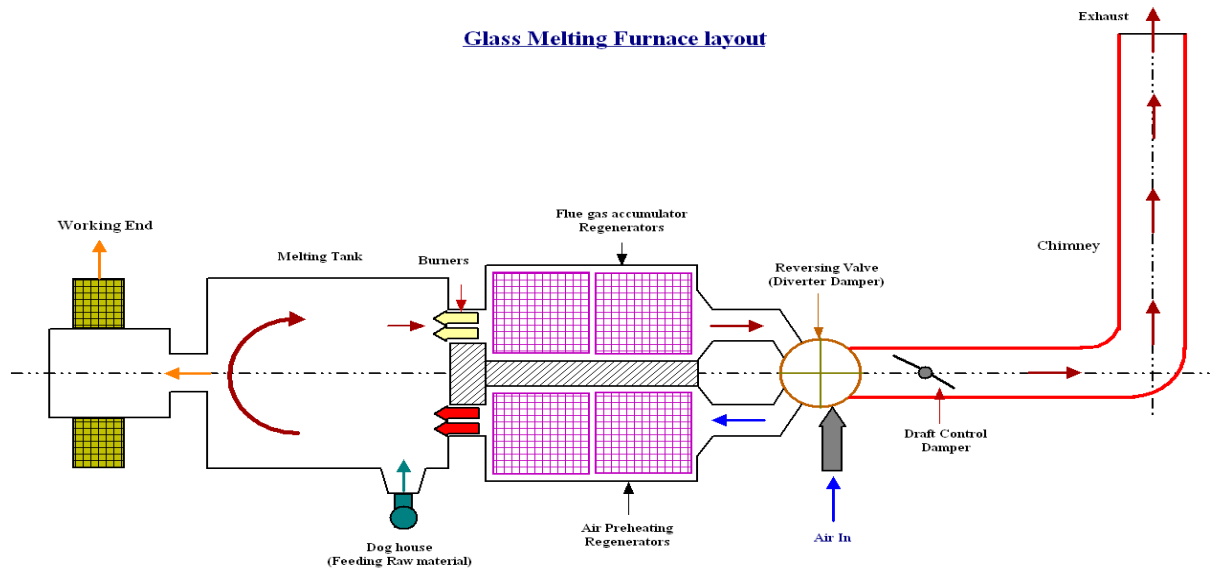


Fig.3.El-Araby Glass Furnace Layout

4. Results and Discussion

4.1 Application on the present modified model

The minimum height required to obtain an adequate dispersion of pollutants is the most important design parameter of industrial chimney. The height and structure of the stack are used to determine the exit temperature of the flue gases and subsequently, the available static draft and the specification of fans. Condensation of water vapor should be prevented which takes place at temperatures of about 40°C, so the corrosion risk still persists because the condensed water entrains dissolved sulfur compounds.

A good design should have an insulation wall in order to avoid wall cold spots in the whole firing range. A glass melting furnace can be regarded as a chemical reactor in which raw materials like silicates, soda ash, etc. are converted from solid state to liquid state. All glass melting reactions is done at high temperature in the range (1450 –1500°C) in a confined space surrounded by refractory wall as shown in figure (3). This figure shows the furnace components, the melting tank, working end and regenerator. The heat is added by using natural gas burners. The furnace capacity is about 90 ton. A regenerator is used to preheat the combustion air. Heat is transferred in this case by convection and radiation.

Some available data and measured parameters of El-Araby glass factory are used as another validation of the present modified model. These data of El-Araby glass melting furnace are presented in table (1) as follows:

| | |
|--|-------|
| Inner diameter D_i (m) | 1.30 |
| Outer diameter (m) | 1.5 |
| Insulation thickness (m) | 0.075 |
| Deposits thickness (m) | 0.015 |
| Gas velocity at chimney exit V (m/s) | 1.313 |
| Inlet gas temperature T_b (°C) | 316 |

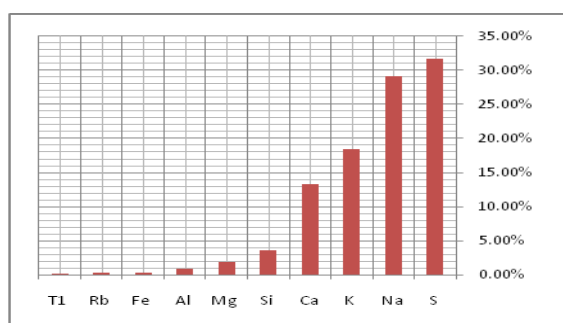


Fig.4. Deposits layer analysis data

| | |
|--------------------------------------|-------------|
| Inner Reynolds number Re_i | 104204.5966 |
| Gas Prandtl number Pr_i | 0.5614 |
| Inner Grashof number Gr_i up to | 10^{10} |
| Stack height L (m) | 45 |
| Ambient temperature T_∞ (°C) | 28 |
| Air Prandtl number Pr_e | 0.7 |
| Outside wall emissivity ϵ_w | 0.9 |

Table.1.El-Araby chimney data

In order to obtain accepted design of stacks, a lot of parameters should be available such as gas velocity or flow rate and inlet temperature which are the input variables. The desired output for given ambient conditions is a quick assessment of the average overall heat transfer coefficient and gas outlet temperature or heat losses.

The steps that should be followed during calculation of the present modified model are presented as follows:

- Flue gases analysis and calculation of thermodynamic properties.
- Internal Nusselt number calculation.
- External Nusselt number calculation.
- Thermal conduction resistances calculation.
- The equivalent Nusselt number calculation.
- The temperature distribution calculation.

The equivalent Nusselt number as a function of internal Nusselt number, external Nusselt number and the thermal conductivity of wall can be presented as follows:

$$\frac{1}{Nu_{eq}(L)} = \frac{1}{Nu_i(L)} + \frac{1}{k_w} \frac{1}{Nu_e(L)} + \frac{1}{2} \frac{k_i}{k_w} \ln \frac{D_e}{D_i} \quad (38)$$

The flue gases out from the glass furnace always carry some of fly ashes materials. These ashes make a layer of deposits or fouling layer on the chimney inside walls. A sample of the formed fouling layer is extracted and has been analyzed in the laboratory and the results of analysis are indicated in figure (4).

This analysis is done by using X-Ray instrument at El-Araby glass factory. This analysis shows that the highest contents are sulfur and sodium. According to [14] the thermal conductivity of fouling may be taken as $k_f = 0.45$ W/m.k.

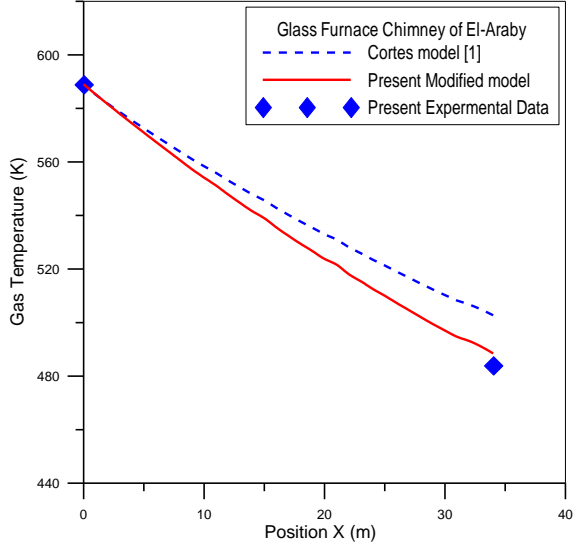
In this case study, the total conduction resistances contain the chimney steel wall resistance, the insulation wall resistance and fouling resistance. The

insulation wall material is aluminum silicate and its thermal conductivity is ($k_{in}=0.9 \text{ W/m.k}$).

4.2 Theoretical and experimental results

Gas temperature distribution

The temperature decay of the flue gases along the chimney wall length is shown in figure (5). The



comparison between the present modified model and Cortes model with the measured data for this case study illustrates that the present modified model is near to the actual measured data. Two points is measured at the chimney inlet and exit.

Fig.5.Flue gas temperature distribution

Inner wall temperature distribution

The outside wall temperature is measured by using laser pyrometer instrument along the chimney outside wall. The inner wall temperature has been calculated based on the measured values of the outside wall by calculating heat transfer at every point. Figure (6) shows that the present modified model is approximately near to the measured data. From this figure, it can be concluded that the present modified model can be considered as a good analytical prediction of the temperature distribution along the inner wall of chimney.

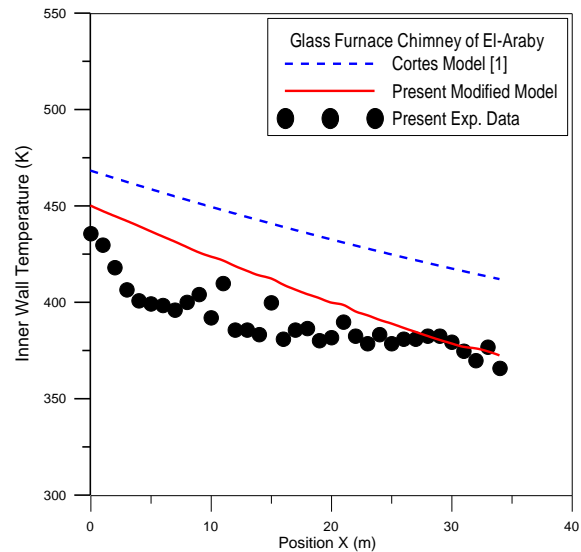


Fig.6. Inner wall temperature distribution

Outside wall temperature distribution

Figure (7) shows the comparison between the measured data of outside wall and the foregoing and present analytical works. The results indicate that the present modified model gives more adequate data and is near to the actual measured data. The measured data are taken along the chimney outside wall at equal distances and at the opposite side of wind direction.

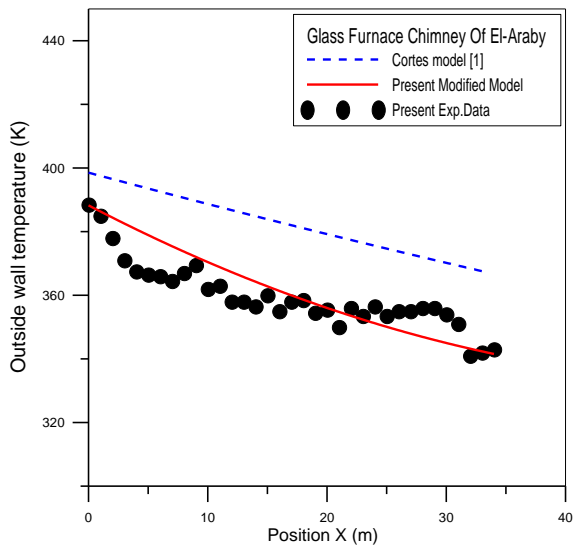


Fig.7. Outer wall temperature distribution

5-Conclusion

Chimney design of industrial furnaces is an important parameter to draught flue gases and heat to the outside atmosphere. The engineering design of industrial chimneys requires prediction of the temperature decay of the industrial combustion gases inside chimneys. An analytical model is developed to obtain accurate heat transfer results.

During this study some parameters are added to Cortes model [1] to have the present modified analytical model such as friction factor and fouling resistance that have considerable effects on both the convection and conduction resistances. The present modified model is applied on the industrial case and it gives a good results. The sequences of calculation are presented. A comparison between the two models and experimental measurements carried out by the authors of this paper is done to show whichever is adequate. Finally, the present modified model can be used by designers to quick prediction of the heat transfer characteristics of chimneys.

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